

## Supporting Materials

### **Enhanced rare earth element recovery from NdFeB leachates using magnetically responsive vermiculite–alginate nanocomposites**

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## 1. Chemicals and Materials

Iron(II) sulfate pentahydrate (99 %, Panreac Quimica S.A., Spain), calcium chloride dihydrate (EMSURE, P.A., Germany), alginic acid sodium salt powder (Sigma Aldrich), potassium hydroxide (P.A., LabChem, USA), potassium nitrate (97.7%, LabChem, USA), and expanded vermiculite (Brazil Minérios S.A., Brazil) were used in the synthesis of the magnetic materials.

The metal solutions were prepared by dissolving their salts in ultrapure water. Salts of Fe(II), Zn(II), Pr(III), Co(II), Nd(III), Dy(III), Mn(II), Ni(II), and Al(III) were used. Details are listed in Table S1.

The eluent solutions were prepared using salts – ammonium chloride ( $\text{NH}_4\text{Cl}$ ), and magnesium(II) dichloride hexahydrate ( $\text{MgCl}_2 \cdot 6\text{H}_2\text{O}$ ) –, complexing agents – diethylenetriaminepentaacetic acid (DTPA), disodium ethylenediaminetetraacetate dihydrate ( $\text{Na}_2\text{EDTA} \cdot 2\text{H}_2\text{O}$ ) –, and strong acids – nitric acid ( $\text{HNO}_3$ ) and hydrochloric acid ( $\text{HCl}$ ). The purities and suppliers of the eluents are compiled in Table S2.

Table S1 REM salts used to prepare the multimetal solution.

Salt	Supplier
Iron(II) sulfate pentahydrate	99 %, Panreac Quimica S.A. (Spain)
Zinc(II) nitrate hexahydrate	99 %, Sigma-Aldrich (Germany)
Praseodymium(III) nitrate hexahydrate	99 %, Sigma Aldrich (Germany)
Cobalt(II) chloride hexahydrate	98 %, Panreac Quimica S.A. (Spain)
Neodymium(III) nitrate hexahydrate	99.9 %, Sigma Aldrich (Germany)
Dysprosium(III) nitrate hexahydrate	99.9 %, Sigma-Aldrich (Germany)
Manganese(II) sulfate monohydrate	99 %, Panreac Quimica (Spain)
Nickel(II) chloride hexahydrate	99.99 %, Merck (Germany)
Aluminum(III) sulfate octadecahydrate	P.A., Pancreac Quimica (Spain)

Table S2 Eluents used in the desorption experiments.

Eluent	Supplier
Ammonium chloride	99.8 %, Pronalab (Portugal)
Magnesium(II) dichloride hexahydrate	P.A., Fagron (Belgium)
Diethylenetriaminepentaacetic acid	97%, Aldrich (Germany)
Disodium ethylenediaminetetraacetate dihydrate	97 %, Fluka (Germany)
Nitric acid	65 %, Applied Chemicals (Switzerland)
Hydrochloric acid	37 %, VWR (USA)

## 2. Modelling methods

### 2.1 Kinetic modeling

Kinetic constants were obtained by nonlinear fitting of the models to the experimental data, such pseudo-first order (PFO, Equation S1) (Lagergren, 1898), pseudo-second order (PSO, Equation S2) (Ho and McKay, 1998a), Elovich (Equation S3) (Aharoni and Tompkins, 1970; Wu et al. 2009), Weber and Morris (Equation S4) (Weber and Morris, 1963) and Boyd (Equation S5-S9) (Boyd et al., 1947; Viegas et al., 2014) models.

$$q_t = q_e(1 - e^{-k_1 t}) \quad (\text{S1})$$

$$q_t = \frac{k_2 q_e^2 t}{1 + k_2 q_e t} \quad (\text{S2})$$

where  $k_1$  (1/min) and  $k_2$  (g/( $\mu\text{mol min}$ )) are the PFO and PSO rate constants,  $q_t$  and  $q_e$  are the solid loadings at a specific time and at the equilibrium ( $\mu\text{mol/g}$ ), and  $t$  is the time (min).

Elovich model is represented by:

$$q_t = \left(\frac{1}{\beta}\right) \ln(1 + \alpha\beta t) \quad (\text{S3})$$

where  $\alpha$  is the initial sorption rate ( $\mu\text{mol}/(\text{g min})$ ), and  $\beta$  is the Elovich constant ( $\text{g}/\mu\text{mol}$ ).

The Weber and Morris model describes sorption kinetics assuming intraparticle diffusion:

$$q_t = k_i \sqrt{t} + I \quad (\text{S4})$$

where  $k_i$  is the rate constant of intraparticle diffusion ( $\mu\text{mol}/(\text{g}\cdot\sqrt{\text{min}})$ ) and  $l$  is the term that refers to the boundary layer (intercept). The higher the  $l$  value, the higher the boundary layer effect on the mass transfer.

The Boyd diffusion model can predict which step limits the mass transfer process of adsorption. According to this method, the solute fraction sorbed up until  $t$  ( $F(t)$ ) can be calculated by:

$$F(t) = \frac{q_t}{q_e} \quad (\text{S5})$$

$$F(t) = 1 - \frac{6}{\pi^2} \sum_{n=1}^{\infty} \frac{1}{n^2} e(-n^2 B_t) \quad (\text{S6})$$

$B_t$  can be calculated by equations S7 and S8 through a simplification of Equation S6 by Fourier transform and numeric integration.

$$0 \leq F \leq 0.85: B_t = 2\pi - \frac{\pi^2 F}{3} - 2\pi \left(1 - \frac{\pi F}{3}\right)^{1/2} \quad (\text{S7})$$

$$0.85 < F \leq 1: B_t = -0.4977 - \ln(1 - F) \quad (\text{S8})$$

The plot of  $B_t$  versus  $t$  specifies the rate-limiting step. If a linear equation fits the data, with null y-intercept, intraparticle diffusion governs the process, otherwise, film diffusion is the rate-limiting step. The angular coefficient ( $B$ ) of the linear fit of  $B_t$  versus  $t$ , is related to the effective diffusivity according to:

$$B = \frac{D_{ef}\pi^2}{r^2} \quad (\text{S9})$$

where  $D_{ef}$  is the effective coefficient of diffusion of the metal on the adsorbent ( $\text{m}^2/\text{min}$ ) and  $r$  is the average size of particles adsorbent (m).

## 2.2 Equilibrium modeling

Equilibrium isotherms with two and three parameters were fitted to data. The two-parameter isotherms are the Freundlich (Freundlich, 1906) (Equation S10), Langmuir (Langmuir, 1918) (Equation S11), and Dubinin-Radushkevich (Equations S12 – S14) (Dubinin and Radushkevich 1947) models.

$$q_e = K_F C_e^{n_F} \quad (\text{S10})$$

$$q_e = \frac{q_{mL} K_L C_e}{1 + (K_L C_e)} \quad (\text{S11})$$

$$q_e = q_{mD} e^{-B_D \varepsilon^2} \quad (\text{S12})$$

$$\varepsilon = RT \ln \left( 1 + \frac{1}{C_e / 10^6} \right) \quad (\text{S13})$$

$$E = \frac{1}{\sqrt{2B_D}} \quad (\text{S14})$$

where  $K_L$  (L/ $\mu$ mol) and  $q_{mL}$  ( $\mu$ mol/g) are the Langmuir constant and sorption capacity, respectively;  $K_F$  ( $\mu$ mol/(g ( $\mu$ mol/L) $^{-1/n_F}$ )) and  $n_F$  are the Freundlich constant and heterogeneity factor, respectively;  $B_D$  is the constant associated with the free energy of adsorption ( $\text{mol}^2/\text{J}^2$ ),  $\varepsilon$  is the Polanyi potential (J/mol),  $R$  is the ideal gas constant (8.314 J/(mol K)),  $T$  is the temperature (K),  $E$  is the free energy of adsorption (J/mol).

The three-parameter models are Brunauer-Emmett-Teller (BET, Equation S15) (Brunauer et al. 1938), Sips (Equation S16) (Sips, 1948) and Toth (Equation S17) (Tóth, 1995, 1997).

$$q_e = \frac{q_{mB}K_B C_e}{(1 - K_u C_e)(1 - K_u C_e + K_B C_e)} \quad (\text{S15})$$

$$q_e = \frac{q_{mS}K_S C_e^{m_S}}{1 + (K_S C_e)^{m_S}} \quad (\text{S16})$$

$$q_e = \frac{q_{mT}C_e}{(K_T + C_e^{t_n})^{1/t_n}} \quad (\text{S17})$$

where  $q_{mB}$  is the sorption capacity of the first layer ( $\mu\text{mol/g}$ ),  $K_B$  is the equilibrium constant of sorption for the first layer ( $\text{L}/\mu\text{mol}$ ), and  $K_u$  is the equilibrium constant of adsorption for upper layers ( $\text{L}/\mu\text{mol}$ );  $q_{mS}$  and  $K_S$  are the Sips maximum capacity ( $\mu\text{mol/g}$ ) and constant ( $\text{L}/\mu\text{mol}$ ), and  $m_S$  is the dimensionless heterogeneity factor;  $q_{mT}$  is defined as the maximum adsorption capacity ( $\mu\text{mol/g}$ ),  $K_T$  is the constant of the Toth equation; and  $t_n$  is a dimensionless parameter known as Toth constant and represents the inhomogeneity of the solid surface and is usually lower than 1. If the value of  $t_n$  equals 1, the Toth model reduces to the Langmuir model, indicating homogeneous sorption.

### 2.3 Assessment of data correlation quality

The statistical parameters to evaluate the goodness of fit of the kinetic models were the adjusted coefficient of determination ( $R^2_{adj}$ ) (Equation S18), the sum of squared errors ( $S_{y,x}$ ) (Equation S19), and the Akaike information criterion (AIC)(Equation S20).

$$R^2_{adj} = 1 - \left[ \frac{(1 - \frac{\sum_{i=1}^N (y_i - \hat{y}_i)^2}{\sum_{i=1}^N (y_i - \bar{y})^2})(N - 1)}{N - K - 1} \right] \quad (\text{S18})$$

$$S_{y,x} = \sqrt{\frac{\sum(\text{residual}^2)}{N - K}} \quad (\text{S19})$$

$$AIC = N \ln \left( \frac{\text{Sum square of errors}}{N} \right) + 2K \quad (\text{S20})$$

where  $N$  is the number of points,  $y_i$  and  $\hat{y}_i$  are the experimental and predicted values, respectively,  $\bar{y}$  is the mean of the experimental values, and  $K$  is the number of estimable parameters plus one (for the variance) (Hurvich and Tsai, 1989).

### 3. Supplementary Figures

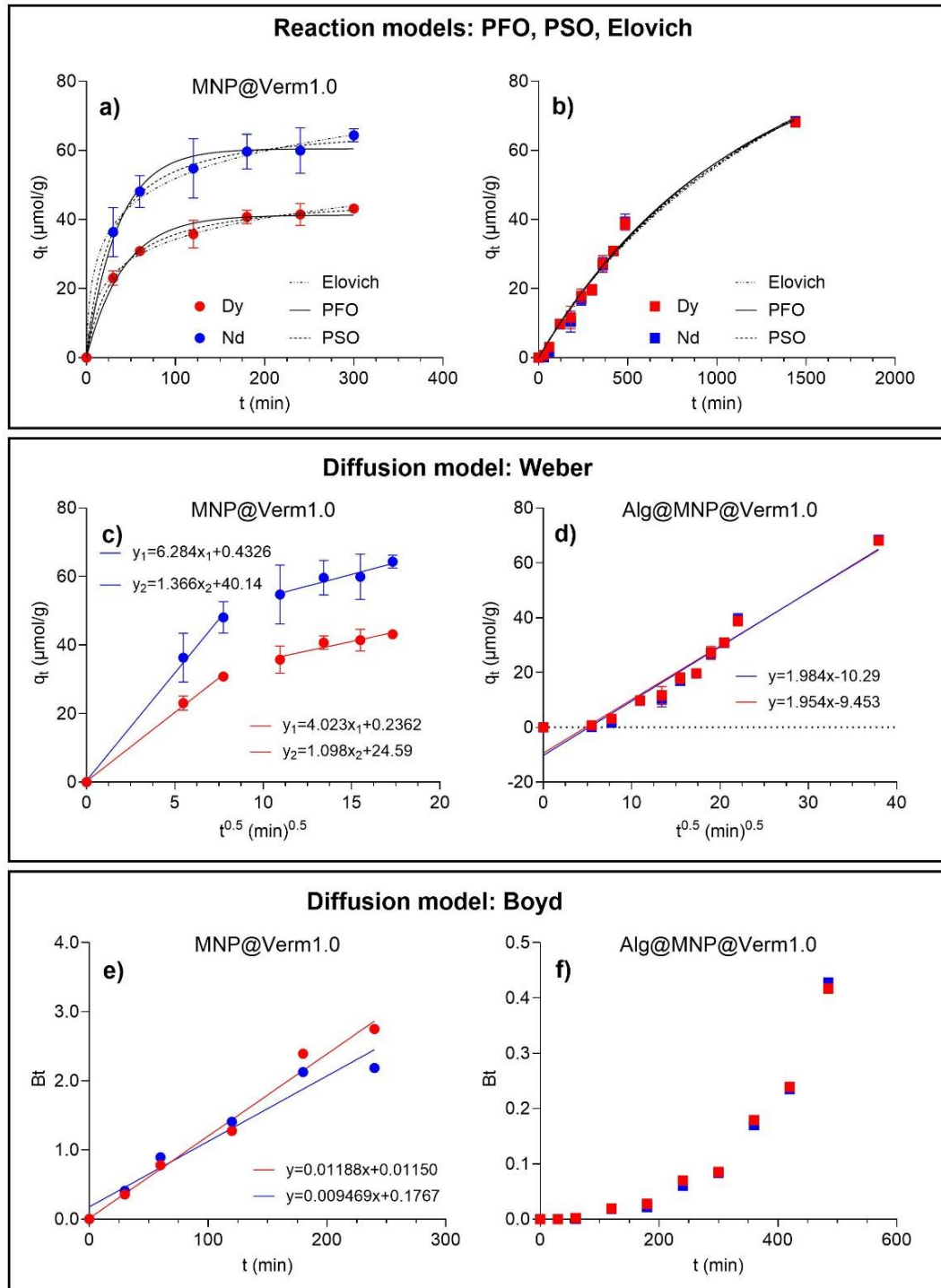


Fig. S1 Sorption of Nd(III) and Dy(III) over time on MNP@Verm1.0 (a, c, and e) and

Alg@MNP@Verm1.0 (b, d, f) nanocomposites, with the corresponding fits of the kinetic models: PFO

and PSO (a and b); Weber and Morris (c and d), and Boyd (e and f)).

## 4. Supplementary Tables

Table S3 Elemental composition (%) of MNP@Verm.10 and Alg@MNP@Verm1.0 determined by SEM-EDS analysis.

Element	Samples	
	MNP@Verm1.0	Alg@MNP@Verm1.0
C	-	18.85
O	47.28	47.8
Mg	6.64	2.97
Al	3.11	1.4
Si	8.18	4.03
Cl	-	0.86
K	1.55	0.17
Ca	-	4.32
Ti	0.23	0.14
Fe	33.01	19.46

Table S4 Best-fit parameters of the reaction and diffusion models.

Model	Parameters	<u>MNP@Verm1.0</u>		<u>Alg@MNP@Verm1.0</u>	
		Nd(III)	Dy(III)	Nd(III)	Dy(III)
<b>Reaction models</b>					
PFO	$k_1$ (1/min)	$2.79 \times 10^{-2}$	$2.39 \times 10^{-2}$	$8.96 \times 10^{-4}$	$9.51 \times 10^{-4}$
	$q_e$ ( $\mu\text{mol/g}$ )	60.4	41.2	95.6	92.2
	$R^2_{adj}$	0.987	0.985	0.980	0.986
	$AIC$	24.9	20.6	30.7	26.0
	$S_{y,x}$	2.58	1.89	2.91	2.35
PSO	$k_2$ ( $\text{g}/\mu\text{mol min}$ )	$5.60 \times 10^{-4}$	$6.51 \times 10^{-4}$	$3.65 \times 10^{-6}$	$4.16 \times 10^{-6}$
	$q_e$ ( $\mu\text{mol/g}$ )	68.1	47.3	154.9	147.2
	$R^2_{adj}$	0.997	0.998	0.978	0.985
	$AIC$	13.7	7.98	31.6	27.2
	$S_{y,x}$	1.16	0.770	3.03	2.48
Elovich	$\alpha$ ( $\mu\text{mol/g min}$ )	10.1	4.13	$8.99 \times 10^{-2}$	$1.74 \times 10^{-2}$
	$\beta$ ( $\text{g}/\mu\text{mol}$ )	$8.64 \times 10^{-2}$	$1.13 \times 10^{-2}$	$1.62 \times 10^{-2}$	$9.30 \times 10^{-2}$
	$R^2_{adj}$	0.995	0.996	0.976	0.983
	$AIC$	18.6	10.8	32.5	28.4
	$S_{y,x}$	1.64	0.938	3.15	2.61
<b>Diffusion models</b>					
<i>1<sup>st</sup> linear segment</i>					
Weber and Moris	$k_i$ ( $\mu\text{mol/g min}^{0.5}$ )	6.28	4.02	1.98	1.95
	<i>intercept</i>	0.433	0.236	-10.3	-9.45
	95% <i>C.I.</i>	-22.6 to 10.5	-12.3 to 12.8	-16.9 to -3.66	-15.5 to -3.42
	$R^2$	0.997	0.998	0.944	0.952
	$S_{y,x}$	1.86	1.02	5.13	4.67
	<i>2<sup>nd</sup> linear segment</i>				
Boyd	$k_i$ ( $\mu\text{mol/g min}^{0.5}$ )	1.37	1.10	n.a.	n.a.
	<i>intercept</i>	40.1	24.6	n.a.	n.a.
	95% <i>C.I.</i>	22.3 to 58.0	8.57 to 40.6	n.a.	n.a.
	$R^2$	0.919	0.902	n.a.	n.a.
	$S_{y,x}$	1.36	1.22	n.a.	n.a.
	<i>slope</i>	0.00947	0.0119	n.a.	n.a.
	<i>intercept</i>	0.177	0.0115	n.a.	n.a.
	$D_{ef}$ ( $\text{m}^2/\text{min}$ )	$1.08 \times 10^{-15}$	$1.36 \times 10^{-15}$	n.a.	n.a.
	95% <i>C.I.</i>	-0.223 to 0.576	-0.276 to 0.300	n.a.	n.a.
	$R^2$	0.951	0.984	n.a.	n.a.
$S_{y,x}$	0.221	0.159	n.a.	n.a.	

Table S5 Equilibrium isotherm models fitted to the sorption of Nd(III) and Dy(III) on MNP@Verm1.0 and Alg@MNP@Verm1.0 nanocomposites.

Model	Parameters	MNP@Verm1.0		Alg@MNP@Verm1.0	
		Nd(III)	Dy(III)	Nd(III)	Dy(III)
<b>Two-parameter isotherms</b>					
Freundlich	$K_F$ ( $\mu\text{mol/g}\cdot(\mu\text{mol/L})^{-1/n_F}$ )	49.2	29.4	44.0	42.6
	$n_F$ (-)	3.35	4.50	2.99	2.89
	$R_{adj}^2$	0.891	0.835	<b>0.961</b>	<b>0.965</b>
	$S_{y,x}$	9.75	6.39	<b>5.84</b>	<b>5.52</b>
	$AIC$	46.1	37.6	<b>40.3</b>	<b>39.3</b>
Langmuir	$q_{mL}$ ( $\mu\text{mol/g}$ )	84.9	44.3	91.8	92.3
	$K_L$ (L/ $\mu\text{mol}$ )	2.39	5.73	0.977	0.897
	$R_{adj}^2$	<b>0.991</b>	<b>0.959</b>	0.917	0.920
	$S_{y,x}$	<b>2.85</b>	<b>3.20</b>	8.51	8.30
	$AIC$	<b>26.4</b>	<b>27.9</b>	47.1	46.6
Dubinin-Radushkevich	$q_{mD}$ ( $\mu\text{mol/g}$ )	76.3	42.5	80.8	80.9
	$B_D$ ( $\text{mol}^2/\text{J}^2$ )	$5.80\times 10^{-8}$	$2.74\times 10^{-8}$	$2.67\times 10^{-7}$	$3.05\times 10^{-7}$
	$R_{adj}^2$	0.961	0.950	0.856	0.852
	$S_{y,x}$	5.82	3.51	11.2	11.3
	$AIC$	37.9	29.2	52.1	52.2
<b>Three-parameter isotherms</b>					
BET	$K_B$ (L/ $\mu\text{mol}$ )	2617	(1)	134	114
	$q_{mB}$ ( $\mu\text{mol/g}$ )	84.4	44.3	58.7	58.4
	$C_S$ (L/ $\mu\text{mol}$ )	1081	$1.20\times 10^{15}$	23.9	24.0
	$R_{adj}^2$	0.989	0.948	0.936	0.942
	$S_{y,x}$	3.12	3.58	7.51	7.09
	$AIC$	35.8	41.9	50.6	49.6
Sips	$K_S$ (L/ $\mu\text{mol}$ )	2.23	4.83	0.360	0.313
	$q_{mS}$ ( $\mu\text{mol/g}$ )	86.1	44.8	174	186
	$n_S$ (-)	0.957	0.926	0.474	0.477
	$R_{adj}^2$	0.989	0.949	0.963	0.966
	$S_{y,x}$	3.08	3.54	5.71	5.46
	$AIC$	35.6	41.8	45.7	44.9
Toth	$q_{mT}$ ( $\mu\text{mol/g}$ )	84.7	53.7	47.6	46.1
	$K_T$ (L/ $\mu\text{mol}$ )	0.416	0.295	0.0313	0.0353
	$t_n$ (-)	1.00	0.908	1.40	1.43
	$R_{adj}^2$	0.989	0.957	0.960	0.964
	$S_{y,x}$	3.12	3.25	5.89	5.60
	$AIC$	35.8	40.6	46.3	45.4

(1) identified as unstable parameter by the analysis software

Table S6 Summary of the XPS binding energies, FWHM (eV), and atomic percentages for the chemical elements detected in MNP@Verm1.0 and Alg@MNP@Verm1.0 before and after the sorption of Nd(III) and Dy(III) (loaded-MNP@Verm1.0 and loaded-Alg@MNP@Verm1.0).

Spectral line	MNP@Verm1.0			Loaded-MNP@Verm1.0		
Name	Peak BE (eV)	FWHM (eV)	Atomic (%)	Peak BE (eV)	FWHM (eV)	Atomic (%)
Al 2p	74.51	2.42	5.6	-	-	-
Al 2s	-	-	-	120.8	4.9	6.59
Si 2s	153.87	3.19	11.78	-	-	-
C 1s	285.18	2.86	6.54	286.34	4.18	5.59
K 2p3	293.92	1.92	0.86	-	-	-
O 1s	531.65	3.46	58.45	532.6	4.65	61.6
F 1s	685.65	2.18	0.44	686.96	3.53	0.49
Fe 2p	711.2	4.69	7.54	711.55	4.34	6.27
Mg 1s	1304.24	2.6	8.79	1305.21	3.34	7.88
Si 2p	-	-	-	104.13	3.65	11.58

Spectral line	Alg@MNP@Verm1.0			Loaded-Alg@MNP@Verm1.0		
Name	Peak BE (eV)	FWHM (eV)	Atomic (%)	Peak BE (eV)	FWHM (eV)	Atomic (%)
Al 2p	73.72	1.73	0.96	-	-	-
Al 2s	-	-	-	119.27	4.89	5.56
Mg 2s	88.46	2.35	1.21	-	-	-
Si 2p	102.1	2.47	3.05	102.35	2.85	6.01
P 2p	-	-	-	133.66	2.66	1.82
Cl 2p	198.29	3.07	3.46	-	-	-
C 1s	285.65	4.52	45.3	285.44	3.57	36.51
Ca 2p3	347.23	2.21	4.7	347.47	2.23	2.08
O 1s	531.98	3.29	39.91	532.12	3.39	43.18
Fe 2p	710.74	6.03	1.16	724.03	4.51	1.3
Cu 2p	-	-	-	953.02	2.88	0.48
Na1s	1071.8	1.38	0.25	-	-	-
Mg 1s	-	-	-	1304.22	2.98	3.07

Table S7 Simulated NdFeB magnet leachate solution, pH = 3.5.

Components	Al	Co	Dy	Fe	Mn	Nd	Ni	Pr	Zn
$C_0$ (mmol/L)	0.034	0.12	0.048	7.27	0.015	0.74	0.026	0.26	0.43

## References of Supporting Information

- Aharoni C, Tompkins FC (1970) Kinetics of Adsorption and Desorption and the Elovich Equation. In: Eley DD; PH; WPB (ed) *Advances in Catalysis*. Academic Press, pp 1–49
- Boyd GE, Adamson AW, Myers LS (1947) The Exchange Adsorption of Ions from Aqueous Solutions by Organic Zeolites. II. Kinetics. *J Am Chem Soc* 69:2836–2848.  
<https://doi.org/10.1021/ja01203a066>
- Brunauer S, Emmett PH, Teller E (1938) Adsorption of Gases in Multimolecular Layers. *J Am Chem Soc* 60:309–319. <https://doi.org/10.1021/ja01269a023>
- Dubinina MM, Radushkevich LV (1947) The equation of the characteristic curve of activated charcoal. *Proceedings of the Academy of Sciences of USSR* 55:331
- Freundlich HMF (1906) Over the Adsorption in Solution. *Journal of Physical Chemistry* 57:385–470
- Ho YS, McKay G (1998) A Comparison of chemisorption kinetic models applied to pollutant removal on various sorbents. *Process Safety and Environmental Protection* 76:332–340.  
<https://doi.org/10.1205/095758298529696>
- Hurvich CM, Tsai CL (1989) Regression and time series model selection in small samples. *Biometrika* 76:297–307. <https://doi.org/10.1093/biomet/76.2.297>
- Lagergren S (1898) About the theory of so-called adsorption of soluble substances. *Kungliga Svenska Vetenskapsakademiens Handlingar* 24:1–39
- Langmuir I (1918) The Adsorption of Gases on Plane Surfaces of Glass Mic and Platinum. *Journal of American Chemical Society* 40:1361–1403
- Sips R (1948) On the structure of a catalyst surface. *J Chem Phys* 16:490–495.  
<https://doi.org/10.1063/1.1746922>
- Tóth J (1995) Uniform interpretation of gas/solid adsorption. *Adv Colloid Interface Sci* 55:1–239.  
[https://doi.org/10.1016/0001-8686\(94\)00226-3](https://doi.org/10.1016/0001-8686(94)00226-3)
- Tóth J (1997) Some Consequences of the Application of Incorrect Gas/Solid Adsorption Isotherm Equations. *J Colloid Interface Sci* 185:228–235. <https://doi.org/10.1006/jcis.1996.4562>
- Viegas RMC, Campinas M, Costa H, Rosa MJ (2014) How do the HSDM and Boyd's model compare for estimating intraparticle diffusion coefficients in adsorption processes. *Adsorption* 20:737–746. <https://doi.org/10.1007/s10450-014-9617-9>
- Weber WJ, Morris JC (1963) Kinetics of adsorption carbon from solutions. *Journal Sanitary Engineering Division Proceedings* 89:31–60
- Wu F-C, Tseng R-L, Juang R-S (2009) Characteristics of Elovich equation used for the analysis of adsorption kinetics in dye-chitosan systems. *Chemical Engineering Journal* 150:366–373. <https://doi.org/10.1016/j.cej.2009.01.014>