

Supporting Information

Appendix A1: The equations of Q_e and AE

The adsorption capacity (Q_e) and adsorption efficiency (AE) of Re(VII) were calculated by the following equations:

$$Q_e = (C_i - C_e) \times V / m \quad (1)$$

$$AE = (C_i - C_e) / C_i \times 100\% \quad (2)$$

where C_i and C_e are the initial and equilibrium concentrations (mg/L) of Re(VII) in the solution, respectively; V is the solution volume (L) and m is the mass of the adsorbent (g).

Appendix A2: Dissolution test

The hydrolytic stability of the ZnO nanoparticles on the surface of biochar was examined via dissolution tests with solution pH range of 1–6. After that, the Zn^{2+} concentrations in the leaching solution were detected using inductively coupled plasma emission spectrometer (ICP-OES, iCAP7400; Thermo Fisher Scientific, USA). The total zinc load on the surface of biochar was measured by the following method: The sample was first heated in a muffle furnace at 750°C for 6 h, and the obtained ash was dissolved in 3 mol/L HCl solution; finally, the Zn^{2+} concentrations in the acidic solution were determined using ICP-OES. As shown in Table 1, negligible amounts of Zn^{2+} in the solution indicated strong stability of ZnO nanoparticles fixation on the biochar surface.

Appendix A3: Water contact angle measurement

Water contact angle measurements were performed on water droplets (drop volume 4 μ L) with an optical contact angle meter (OCA25; Dataphysics, Germany) at room temperature. Deionized water was used as a probe liquid and when deionized water droplet of 4 μ L was put on the carbonaceous adsorbent surface, the water contact angle was averaged at five points of each sample.

Appendix A4: Point of zero charge determination

The point of zero charge (pH_{pzc}) of the biochar were determined as described by the previous study (Zhu et al., 2014): 1) 10 mL NaCl solution (0.01 mol/L) was placed in a 20 mL glass bottle to maintain the ion strength of the solution, 2) the pH of solution was adjusted ranged from 2.0 to 10.0 at pH intervals of 1 by using 0.1 mol/L of HCl or NaOH solution, 3) 0.02 g biochar was added into the solution and the mixtures were then vigorously shaken at 130 r/min and 25°C for 48 h, 4) the supernatant was decanted and the final pH of solution was measured by using a calibrated pH meter (PHS-3C, Shengbang, China). The pH_{pzc} from each set were calculated based on the ΔpH (final-initial pH) = 0.

Appendix A5: pH of biochar measurement

The pH value of biochar was measured according to previous literature using 1 g of biochar in 20 mL of deionized water, which was shaken at 140 r/min for 24 h on a temperature controlled shaker (Wang et al., 2015). The solution was measured by a calibrated pH meter (PHS-3C; Shengbang, China).

Table S1 The element ratio of ZBC

Element	Wt %
C	40.787
O	5.304
Si	21.035
Zn	32.873

Table S2 Adsorption isotherm and kinetic models used in the study

Models	Names	Equations
Isotherm models	Langmuir	$Q_e = \frac{Q_m K_L C_e}{1 + K_L C_e}, \quad R_L = \frac{1}{1 + K_L C_m}$
	Freundlich	$Q_e = K_F C_e^{1/n}$
	Temkin	$Q_e = \frac{RT}{B_T} \ln(K_T C_e)$
Kinetic models	pseudo-first-order	$Q_t = Q_e (1 - \exp(-K_1 t))$
	pseudo-second-order	$Q_t = \frac{K_2 Q_e^2 t}{1 + K_2 Q_e t}$
	Elovich	$Q_t = \frac{1}{\beta} \ln(1 + \alpha \beta t)$
	intra-particle diffusion	$Q_t = K_{id} t^{0.5} + C$
	liquid film diffusion	$\ln(1 - F) = -K_{lf} t, \quad F = \frac{Q_t}{Q_e}$

Notes: Q_e is adsorption capacity (mg/g) at equilibrium time; Q_m is maximum adsorption capacity (mg/g); K_L is Langmuir constant; C_m is highest initial Re concentration (mg/L); K_F and n are Freundlich constants; R is universal gas constant (8.314 J/(mol·K)); T is absolute temperature (K); B_T is Temkin constant (kJ/mol); K_T is equilibrium bond constant related to the maximum energy of bond; Q_t is adsorption capacity (mg/g) at time t ; K_1 and K_2 are rate constants of the pseudo-first-order and pseudo-first-order models, respectively; α and β are Elovich constants; C and K_{id} are intraparticle diffusion constants (mg/g, (mg·h^{0.5})/g); K_{lf} is adsorption rate constant

Table S3 Kinetic parameters for the adsorption of Re(VII) onto BC and ZBC

Kinetic models	Parameters	BC	ZBC
Experimental	$Q_{e,exp}$	3.58	5.86
Pseudo-first-order	$Q_{e,cal}$	3.37	5.25
	K_1	0.2684	1.2797
	R^2	0.8972	0.8550
	RSS	0.1310	0.2830
Pseudo-second-order	$Q_{e,cal}$	3.84	5.61
	K_2	0.0987	0.3308
	R^2	0.9456	0.9606
	RSS	0.0693	0.1062
Elovich	$Q_{e,cal}$	3.56	5.86
	α	4.7396	113.8923
	β	1.4314	1.4031
	R^2	0.9734	0.9979
	RSS	0.0338	0.0057
Intraparticle diffusion	K_{id}	0.7911	3.1120
	C	0.6343	0.6277
	R^2	0.9674	0.9409
	RSS	0.2374	0.4319

Table S4 Isotherm parameters for the adsorption of Re(VII) onto BC and ZBC

Isotherm models	Parameters	BC	ZBC
Langmuir	Q_m	13.72	29.41
	K_L	0.0330	0.0959
	R^2	0.9775	0.9608
	RSS	0.1723	2.2733
Freundlich	K_F	1.8414	6.7245
	n	2.6586	3.1403
	R^2	0.9572	0.9866
	RSS	0.3273	0.7791
Temkin	K_T	0.3590	1.9153
	B_T	0.3430	0.1926
	R^2	0.9767	0.9812
	RSS	0.1783	1.0888

Table S5 Thermodynamics model used in the study

Model	Equations
	$\Delta G^\circ = -RT \ln K$
Thermodynamics models	$\ln K = -\frac{\Delta H^\circ}{RT} + \frac{\Delta S^\circ}{R}$

Notes: R is universal gas constant (8.314 J/(mol·K)); T is absolute temperature (K); K is the thermodynamic equilibrium constant

Table S6 Thermodynamic parameters for the adsorption of Re(VII) onto ZBC

Thermodynamic parameters	Values
ΔG° (kJ/mol)	-0.19 (298.15 K)
	-1.13 (303.15 K)
	-2.07 (308.15 K)
	-3.01 (313.15 K)
ΔH° (kJ/mol)	55.90
ΔS° (J/(mol·K))	188.12

References

Wang Z, Liu G, Zheng H, Li F, Ngo H H, Guo W, Liu C, Chen L, Xing B (2015). Investigating the mechanisms of biochar's removal of lead from solution. *Bioresource Technology*, 177: 308–317

Zhu X, Liu Y, Qian F, Zhou C, Zhang S, Chen J (2014). Preparation of magnetic porous carbon from waste hydrochar by simultaneous activation and magnetization for tetracycline removal. *Bioresource Technology*, 154: 209–214