

Electronic Supplementary Material

Chemical reactions of oily sludge catalyzed by iron oxide under supercritical water gasification condition

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E-mail: yhan@tju.edu.cn Simulation temperature

Voter et al.[1] had presented a method that raising the temperature could accelerate the reaction process with extending the time scale by orders of magnitude, which has become a common simulation strategy for ReaxFF MD in a limited time scale. Likewise, according to Arrhenius equation ($k=Ae^{-E_a/(k_B T)}$), raising temperature could accelerate the reaction rate without changing the activation energy barrier, which means the higher the temperature, the faster the reaction happens, and the shorter the time it takes to reach chemical equilibrium. Thus, the chemical reaction could reach equilibrium in a limited time scale compared with the reaction time at normal reaction temperature. For example, Xia et al.[2] investigated the depolymerization process and reaction pathways of scrap tires in SCW condition via ReaxFF MD, and the weight percentages of solid residues combined experiments and

simulations at different temperature (473.15 – 703.15 K vs 1400 – 2600 K) and reaction times (min vs ps) summarizing in the equation:

$$Tr = \frac{Ts + 3087.41}{7.94}$$

so the phenomenon in the smaller time scale and higher temperature simulations can match the phenomenon in the experiments with larger time scale and lower temperature. Wang et al.[3] investigated the carbonization of C₂H₄ on iron nanoparticles at 2500 K and ns scale using ReaxFF MD. Jin et al.[4] adopted a temperature of over 3500 K to figure out the coal gasification process with ns scale in SCW by ReaxFF MD. Zhang et al.[5] applied 3000 K and 800 ps for studying the mechanism of naphthalene degradation on iron oxide in SCWG process. Herein, the simulation always adopts higher temperature in limited time scale. Furthermore, the addition of catalyst could moderate the extreme operation conditions. Therefore, the temperature selected in this study was 2300 K, which is lower compare to the above works.

Descriptions for Figure 10(a) and 10(d)

With the addition of Fe clusters into the system, Fe clusters would be adsorbed on the surface of Fe₂O₃ catalyst providing more active sites, it can adsorb not only reactants, but also more H₂O molecules to generate more •H and •OH radicals, the intuitive phenomena are that the amounts of H₂O molecules are decreased and the output of H₂ molecules is risen. And the generation of CO₂ is reliable on sufficient lattice oxygen, and the exposed lattice oxygen is decreased when Fe clusters are

adsorbed on Fe_2O_3 , then, large amounts of $\cdot\text{H}$ radicals are generated due to more Fe active sites exposed, which reduces the probability of CO being oxidized to form CO_2 . Herein, Figure 10(a) and 10 (d) could exhibit the synergistic effect.

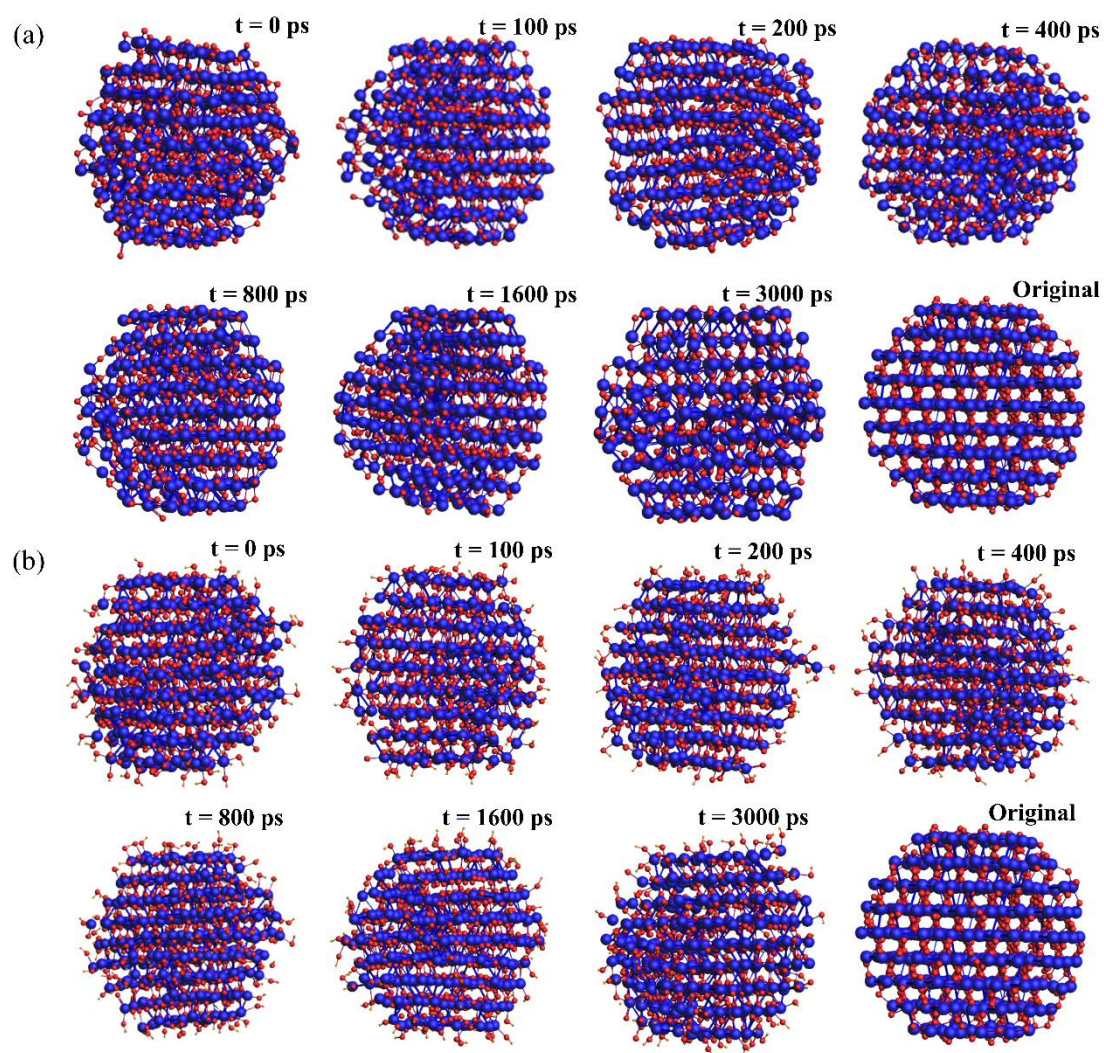


Figure S1. Change of crystal morphology of Fe_2O_3 during (a) pyrolysis; (b) SCW conditions

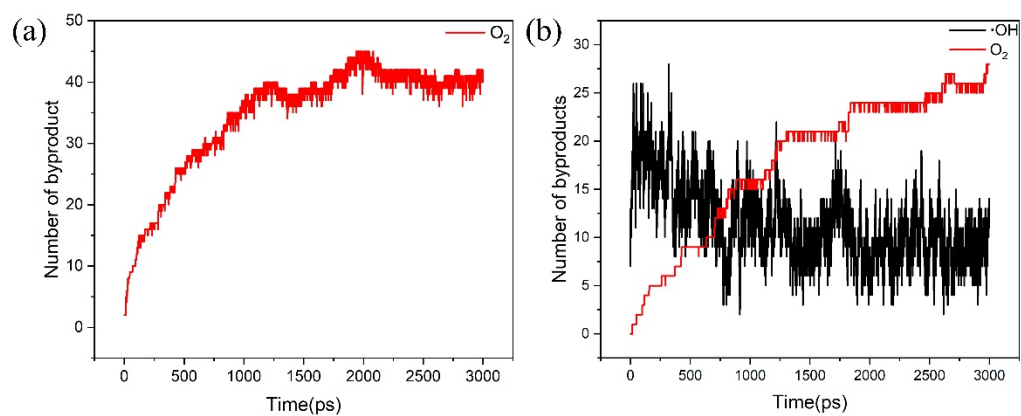


Figure S2. Byproducts produced by (a) pyrolysis; (b) SCW conditions of Fe_2O_3 crystal

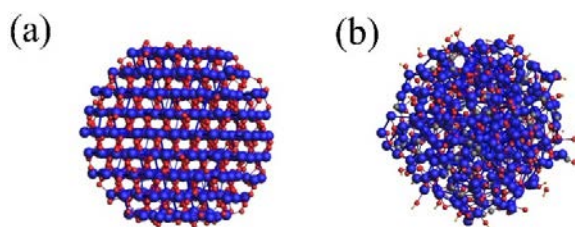


Figure S3. Morphology of (a) fresh; (b) used catalyst;

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