

Stability of Ni/SiO₂-ZrO₂ catalysts towards steaming and coking in the dry reforming of methane with carbon dioxide

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Supporting Information

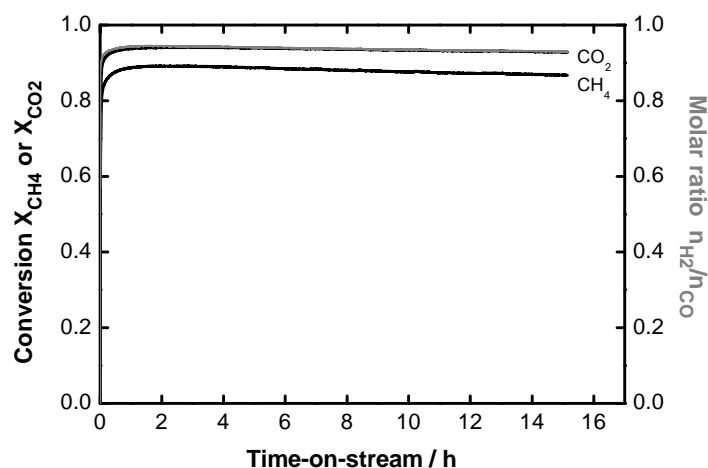


Fig. 1S CH₄ and CO₂ conversion as well as molar ratio $n_{\text{H}_2}/n_{\text{CO}}$ as a function of time-on-stream in the DRM over Pt/ZrO₂ (T = 850 °C, GHSV = $6.0 \times 10^3 \text{ h}^{-1}$, $n_{\text{CH}_4}/n_{\text{CO}_2}/n_{\text{Ar}} = 47.5/47.5/5.0$).

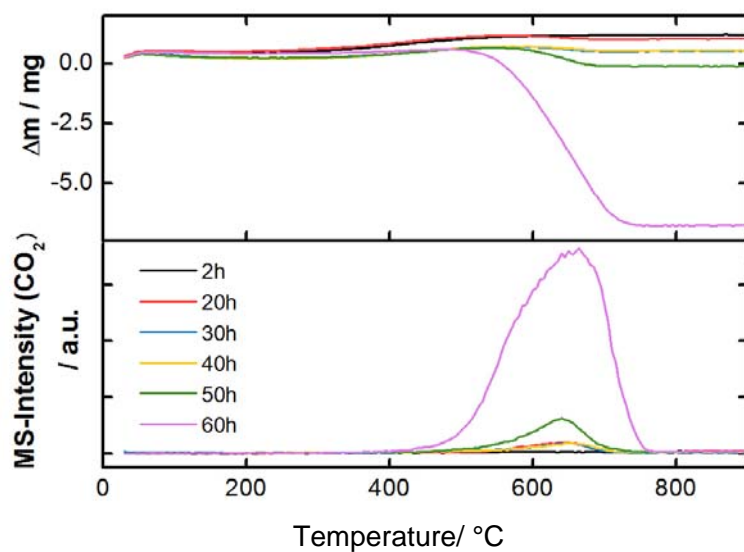


Fig. 2S TGA-profiles (top) and MS-intensity for CO₂ (bottom) during TGA for 5Ni/SiO₂-ZrO₂ (batch 1) after DRM for different times-on-stream (T = 850 °C, GHSV = 1.8×10³ h⁻¹, n_{CH₄}/n_{CO₂} = 1/1).

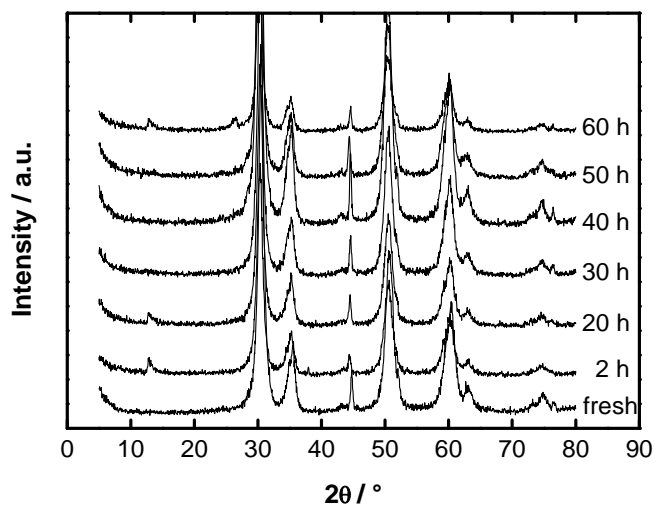


Fig. 3S PXRD patterns of 5Ni/SiO₂-ZrO₂ (batch 1) before (fresh) and after different times-on-stream in DRM (T = 850 °C, GHSV = 1.8×10³ h⁻¹, n_{CH₄}/n_{CO₂} = 1/1).

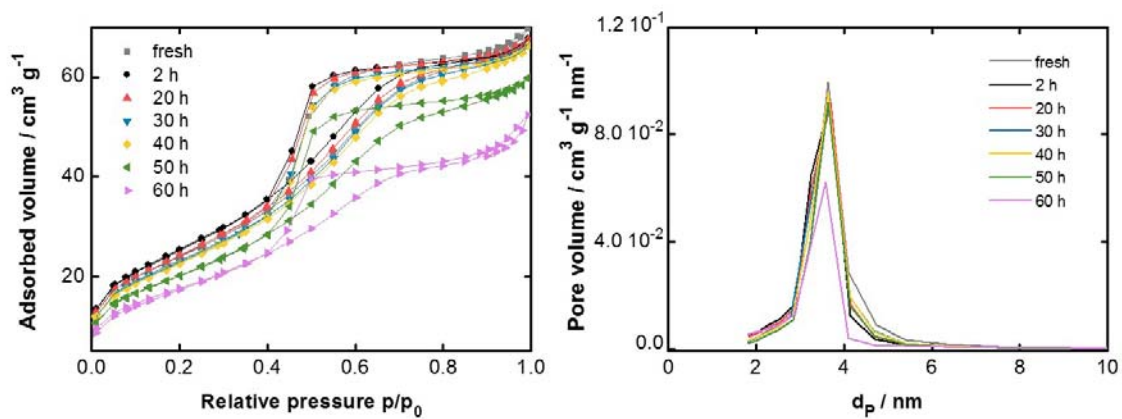


Fig. 4S N₂-Sorption isotherms (left) and pore width distribution (from the desorption branch of the isotherms; right) of 5Ni/SiO₂-ZrO₂ (batch 1) before (fresh) and after different times-on-stream in DRM (T = 850 °C, GHSV = 1.8×10³ h⁻¹, n_{CH₄}/n_{CO₂} = 1/1).

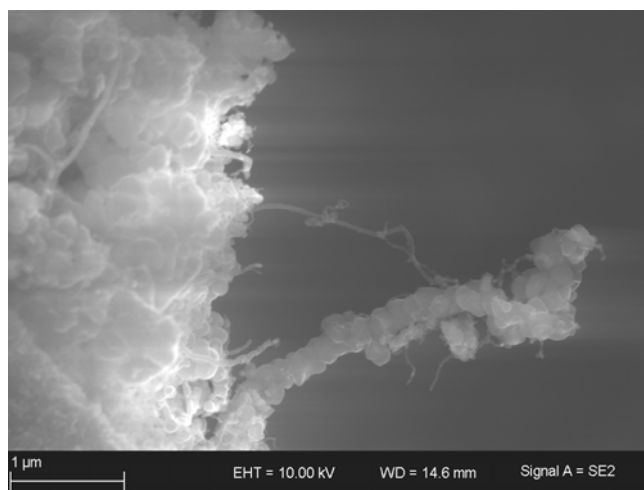


Fig. 5S SEM image of 5Ni/SiO₂-ZrO₂ (batch 1) after 60 h on-stream in DRM (T = 850 °C, GHSV = 1.8×10³ h⁻¹, n_{CH₄}/n_{CO₂} = 1/1).

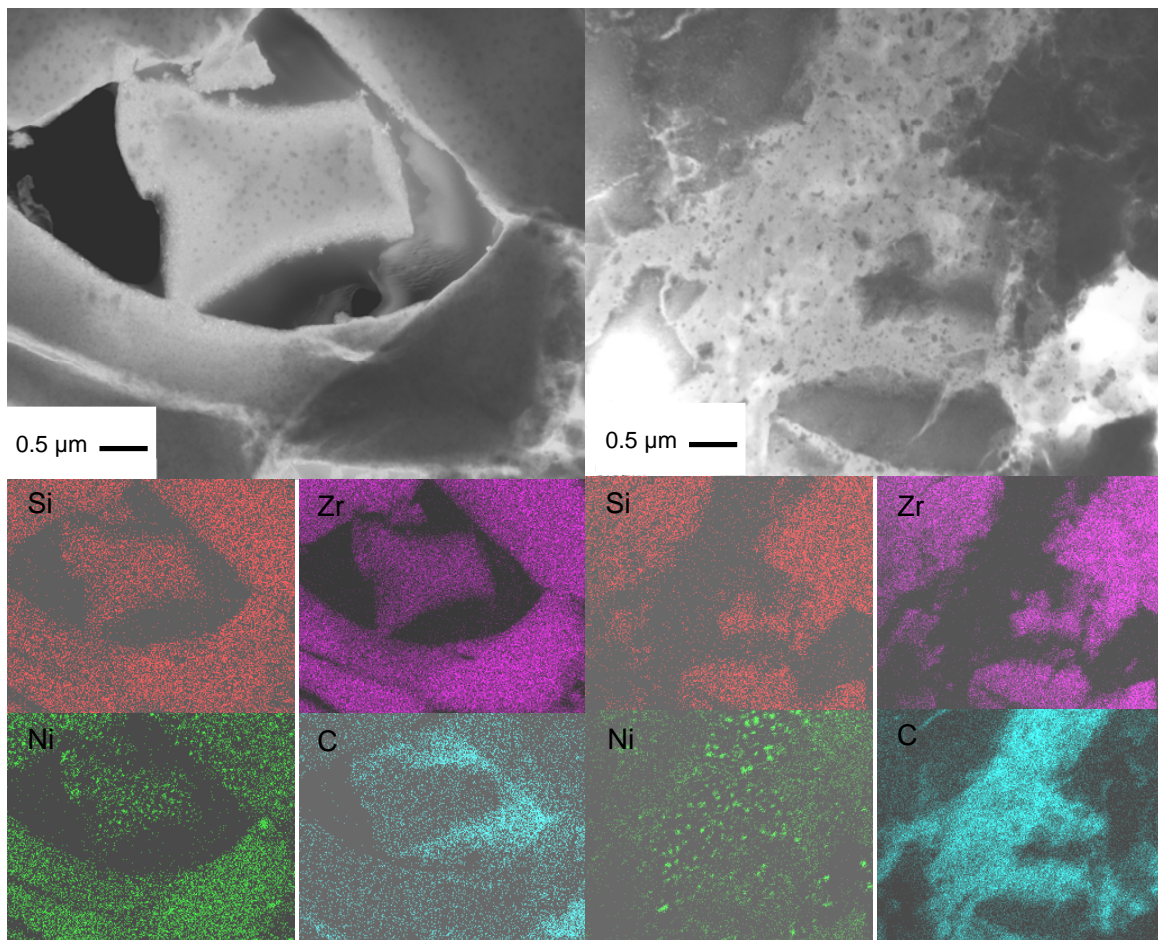


Fig. 6S STEM dark-field image of 5Ni/SiO₂-ZrO₂ (batch 1) after 2 h on-stream (left) and bright-field image of 5Ni/SiO₂-ZrO₂ (batch1) after 60 h on-stream in DRM (T = 850 °C, GHSV = 1.8×10³ h⁻¹, n_{CH₄}/n_{CO₂} = 1/1). The bottom part shows EDX maps of the same image areas for Si, Zr, Ni and C.

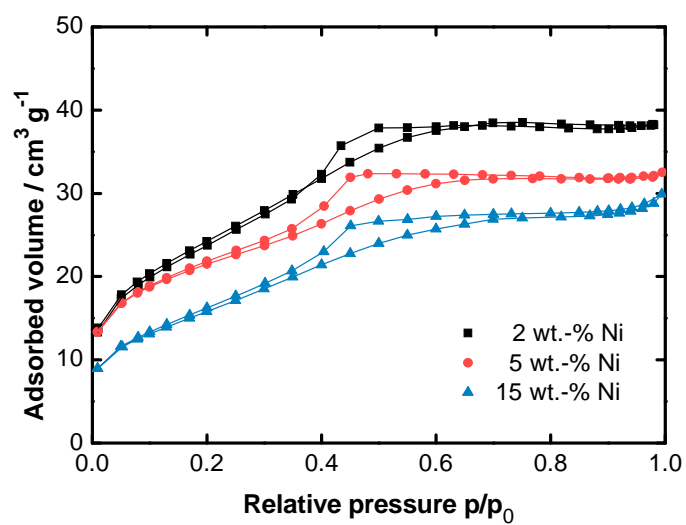


Fig. 7S N₂-Sorption isotherms of Ni/SiO₂-ZrO₂ (batch 2; fresh) with different Ni loadings.

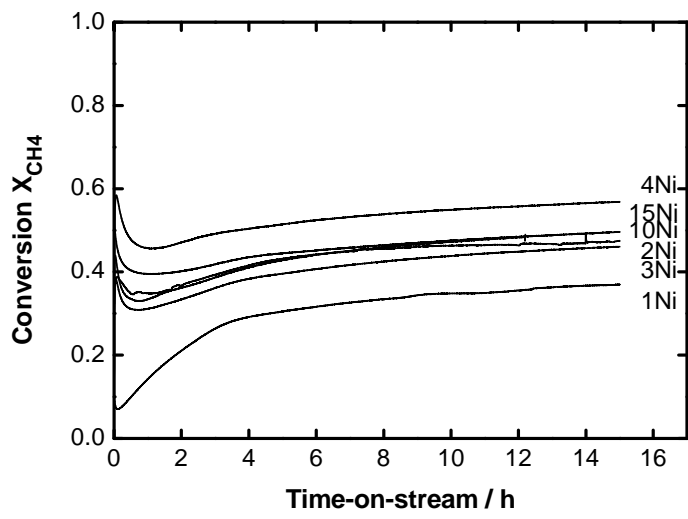


Fig. 8S CH₄ conversion as a function of time-on-stream in the DRM over Ni/SiO₂-ZrO₂ (batch 2) with different Ni loadings (T = 850 °C, GHSV = 6.0 × 10³ h⁻¹, n_{CH₄}/n_{CO₂}/n_{Ar} = 47.5/47.5/5.0).