

COMMUNICATION

Monodispersed Cu-TCPP/Cu₂O Hybrid Microspheres: A Superior Cascade Electrocatalyst Toward CO₂ Reduction to C₂ Products

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Abstract

The electrochemical conversion of carbon dioxide (CO₂) into valuable chemicals is a feasible way to mitigate the negative impacts of overmuch CO₂ emissions. Porphyrin-based metal organic frameworks (MOFs) are expected to be used for selective and efficient electrochemical CO₂ reduction (ECR) with porous structure and ordered active sites. Herein, we report the synthesis of a monodispersed and spherical organic/inorganic hybrid Cu-TCPP@Cu₂O electrocatalyst composed of Cu-TCPP (TCPP = tetrakis (4-carboxyphenyl) porphyrin) and Cu₂O, where TCPP plays significant roles in regulating the morphology. *In-situ* formed Cu during ECR process in combination with Cu-TCPP (Cu-TCPP@Cu) can suppress hydrogen evolution, enrich CO intermediate and promote C–C coupling toward C₂ products. The Cu-TCPP@Cu supported on porous carbon (PC) showed ultrafine Cu nanoclusters on PC, and displayed high ECR activity and selectivity toward C₂ products, with a C₂ faradaic efficiency of 62.3% at –1.0 V versus the reversible hydrogen electrode and a C₂ partial current density of 83.4 mA·cm^{–2}, which is 7.6 times and 13.1 times those of pure Cu₂O and TCPP, respectively. The morphology and hybrid structure of the catalyst were studied to improve the selectivity of ECR to produce C₂ products, which provides a new idea for the design of high-performance ECR catalyst.

Keywords: Organic/inorganic hybrid electrocatalysts; TCPP; Cuprous oxide; Cascade electrocatalysts

1. Introduction

Human activities lead to excessive emission of carbon dioxide (CO₂) into the atmosphere, resulting in serious environmental and climate problems, such as glacier melting and greenhouse effect [1–4]. Powerful methods of storing and converting CO₂ have been developed to reduce CO₂ levels in the atmosphere [5–8], among which, renewable energy driven electrocatalytic reduction of CO₂ (ECR) into valuable multi-carbon products is one of the promising and sustainable approaches [9–12]. However, catalysts limit the

efficiency and selectivity of electrochemical CO₂ reduction [13–15]. Therefore, people have been committed to the development of a variety of efficient selective conversion of CO₂ electrocatalysts [16,17], like metal oxides [18,19], carbon-based materials [20] and metal organic frameworks (MOFs) [21,22]. Despite the significant progress, it remains a huge challenge to direct the reaction path to the ideal product, which requires the development of better electrocatalysts with higher product selectivity and catalytic activity [23–25].

MOF is regarded as an advantageous ECR electrocatalyst because of its porous crystalline

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structure and CO₂ affinities [26,27]. Therefore, a large number of molecular catalysts combining transition metal (TM) elements (like Fe, Co, Ni, Mn and Cu) with macrocyclic ligands (such as polypyridine, porphyrins and phthalocyanine) have been examined for the electrochemical reduction of CO₂ [28]. For instance, Chi and co-workers synthesized a kind of porous three-dimensional porphyrinic cobalt MOF with a CO faradaic efficiency of 92.4% at -0.6 V vs. reversible hydrogen electrode (RHE) [29]. In addition, Kongpatpanich [30] prevented the aggregation of porphyrins by embedding functionalized cobalt-based and iron-based porphyrins into rigid frame structures, and ensured that the H bond interface was only close to the intermediate products of ECR at the same time, thus reducing the limit potential of ECR and improving the selectivity of ECR. Besides, Su's team synthesized a series of structurally stable metallic two-dimensional (2D) polyoxometal-metalloporphyrin organic frameworks (TM-PMOFs, TM = Fe, Co, Ni, Cu, Zn, Ru, Rh, Pd, Os, Ir, Pt). Their calculations showed that Lindqvist type clusters [Mo₆]^{2e/2H} can act as a multi-electron regulator of the reduction reaction, reducing the drive potential of the reaction (0.08 V) [31]. Unfortunately, considering the completion of the multi-electron transfer process required to obtain any reduced product in ECR, the poor conductivity and electron-donating capacity of MOF have always been a major limitation of MOF as an efficient electrocatalyst [32]. Therefore, it is imperative to design a novel catalyst with active components, electron-rich units and electron mobility.

At present, metals [33–35], metal sulfides [36], organic groups [37] and metal oxides [38–40] have been combined with porphyrin complexes to improve their activity and produce synergistic effects. Tetrakis (4-carboxyphenyl) porphyrin (TCPP) is a kind of electron donor which has been used to improve the ECR performances of MOFs [41]. Electron transfer could be facilitated by integrating electron-rich units into porphyrin-based MOFs, which could obtain excellent ECR activity. For example, Chang and colleagues reported a urea pendant modified molecular iron porphyrin catalyst with high CO faradaic efficiency, and the catalytic rate was 1500 times that of the unmodified parent iron porphyrin [42].

In addition, Zheng's group also developed a donor-acceptor modified Cu porphyrin (Cu-TAPP), which exhibited an excellent CO₂-to-CH₄ electroreduction performance, including a high CH₄ partial current density of 290.5 mA·cm⁻² and a corresponding faradaic efficiency of 54.8% at -1.63 V vs. RHE in flow cells [43]. Liang's team [44]

also synthesized nickel phthalocyanine (NiPC-MDE) with methoxy (-OMe) and cyanide (-CN). Compared with cyano-substituted NiPC-CN-MDE, the methoxy-substituted NiPC-OMe-MDE catalyst can stabilize *COOH intermediates and improve the selectivity of CO. The NiPC-OMe-MDE catalyst could maintain 99.5% CO selectivity in the current density range of 10–300 mA·cm⁻². Although these materials can effectively promote the catalysis of electrochemical reduction of CO₂, the ECR C₂ products are still very limited. Promoting the multi-electron transfer reactions with high selectivity of C₂ products remains a grand challenge for molecular-based electrocatalysts.

Herein, we report the deliberate synthesis of monodispersed and spherical organic/inorganic hybrid Cu-TCPP@Cu₂O, composed of 2-dimensional Cu-TCPP and Cu₂O, which can be converted to Cu-TCPP@Cu during the ECR process and displays a faradaic efficiency of 62.3% at -1.0 V vs. RHE. Our study shows that the interaction between Cu-TCPP and Cu₂O is the key factor contributing to its excellent ECR performance.

2. Experimental section

2.1. Materials

Tetrakis (4-carboxyphenyl) porphyrin (TCPP, 97%), zinc nitrate hexahydrate (Zn(NO₃)₂·6H₂O, 98%), trifluoroacetic acid (99%) and copper nitrate trihydrate (Cu(NO₃)₂·3H₂O, 99%) were purchased from Macklin. N, N-dimethylformamide (DMF, 99.9%), methanol, ethanol, 2-methylimidazole, potassium hydroxide (KOH, 95%) and polyvinylpyrrolidone (PVP, average mol. wt. 50,000) were purchased from Energy Chemical Co. Deionized water (DI, 18.2 MΩ·cm) was acquired from Milli-Q system. All agents were analytically pure and used without further purification.

2.2. Preparations of Cu-TCPP@Cu₂O and contrastive samples

2.2.1. Synthesis of Cu-TCPP@Cu₂O nanoparticles

A solution made of TCPP (20 mg, 0.025 mmol) and PVP (500 mg) in DMF (16 mL) was added to a solution of Cu(NO₃)₂·3H₂O (121.91 mg, 0.65 mmol) in DMF (10 mL). The mixed solution was refluxed for 24 h at 120 °C after stirring for 2 min [45]. After cooling down to room temperature, the resulting red Cu-TCPP@Cu₂O nanoparticles were washed four times with DI water and collected by centrifuging at 8500 rpm for 5 minutes.

The synthesis process of pure Cu₂O was the same as that of Cu-TCPP@Cu₂O without TCPP.

The synthesis process of pure Cu-TCPP was the same as that of Cu-TCPP@Cu₂O except for the addition of trifluoroacetic acid (20 μ L, 1.0 mol·L⁻¹).

In addition, the catalysts after ECR corresponding to Cu-TCPP@Cu₂O, Cu₂O, Cu-TCPP and TCPP are named as Cu-TCPP@Cu, OD-Cu, Cu-TCPP spent and TCPP spent, respectively, while the corresponding samples mixed with porous carbon (PC) are named as Cu-TCPP@Cu₂O/PC, Cu₂O/PC, Cu-TCPP/PC and TCPP/PC.

2.2.2. Synthesis of porous carbon by carbonization of ZIF-8

The Zn(NO₃)₂·6H₂O (5.94 g, 0.02 mol) and 2-methylimidazole (6.56 g, 0.08 mol) were added into methanol (500 mL). After mixing for 12 h at room temperature, the formed ZIF-8 nanoparticles were washed for three times with methanol and collected by centrifuging at 8500 rpm for 3 minutes.

The ZIF-8 (500 mg) was put at a porcelain boat in a quartz tube furnace. Subsequently, the temperature of the tube furnace was elevated to 950 °C with a heating rate of 5 °C·min⁻¹ under Ar atmosphere and held at this temperature for 3 h. The obtained porous carbon is named as PC.

2.3. Morphological and structural characterizations

Powder X-ray diffraction (Bruker D8 Advanced, German) test was performed using a Cu K_α radiation source. X-ray photoelectron spectroscopic (XPS) measurements were performed on a PHI X-tool X-ray photoelectron spectrometer using Al as the exciting source. Scanning electron microscopic (SEM) images and the elements distribution of the catalyst were recorded using a Zeiss Supra 55. Transmission electron microscopic (TEM) images were obtained on a Talos F200x.

2.4. Electrochemical characterization

Electrochemical CO₂ reduction tests were performed on a CHI 660E electrochemical analyzer using a designed gas-tight flow cell. None of the electrochemical tests in this work used IR compensation. The platinum foil counter electrode was purchased from Sigma Aldrich. The Hg/HgO reference electrode and carbon fiber paper were purchased from Gaoss Union. The conversion of the Hg/HgO electrode to the reversible hydrogen electrode (RHE) is performed using the following formula [46]:

$$E_{\text{RHE}} = E_{\text{Hg/HgO}} + 0.095 \text{ V} + 0.059 \times \text{pH}$$

Firstly, a diluted Nafion solution was prepared by mixing 5 mL DI water, 5 mL ethanol and 0.5 mL

Nafion solution (5% *w/w*). Disperse 2.5 mg of Cu-TCPP@Cu₂O catalyst and 2.5 mg PC into 5 mL of the diluted Nafion solution, by sonication for 30 min to obtain a catalyst ink. Drop-cast 1 mL the catalyst ink onto each carbon paper with gas diffusion layer (GDL) to obtain the catalyst-loaded gas diffusion electrode (GDE, 2 cm × 0.5 cm). The geometric area of each electrode is 1 cm² and the catalyst loading on each electrode was controlled to be 1.0 mg·cm⁻². The working electrodes for pristine Cu₂O/PC, Cu-TCPP/PC and TCPP/PC were prepared by following the same procedure as that of Cu-TCPP@Cu₂O/PC.

For all experiments, 1.0 mol·L⁻¹ KOH (pH = 14) solution was used as the electrolyte. The durability was evaluated by chronoamperometric profiles at a constant current density. The double-layer capacitance (*C_{dl}*) values and electrochemical surface area (ECSA) were determined by cyclic voltammetric (CV) curves at different scanning rates. Electrochemical impedance spectroscopic (EIS) measurements were made at frequencies ranging from 100 kHz to 0.01 Hz in a potentiostatic mode. Current densities were calculated based on the catalyst-covered geometric area of the working electrode. All potentials reported in this work are referred to RHE. The liquid product of ECR was quantified by ¹H NMR spectra recorded with an Agilent 400 MHz NMR instrument. The gas product generation of ECR was calculated by gas chromatography with an HuaAi GC-9560.

3. Results and discussion

The morphology of Cu-TCPP@Cu₂O was examined by SEM and TEM. In Fig. 1a, Cu-TCPP@Cu₂O exhibits a spherical shape and a bumpy surface, with a size of 2.78 ± 0.67 μ m in diameter (Fig. S1a–b). It is highly possible that the bumpy surface of Cu-TCPP@Cu₂O was assembled with ultrathin nanosheet of Cu-TCPP [47]. The element mapping for Cu-TCPP@Cu₂O demonstrates the uniform distribution of each element on the sample. The high-resolution TEM image of Cu-TCPP@Cu₂O (Fig. 1b) further indicates the rough surface, composed of small nanoparticles at 3–5 nanometres. The lattice fringe at the heart of the sample was identified to be 0.2464 nm (Fig. 1c), which agrees with Cu₂O (1 1 1) reflection [47]. Similarly, the pristine Cu₂O sample without TCPP functionalization equally shows spherical shape, and two-size distribution in diameter, i.e., 96.56 and 264.74 nm, which are much smaller than that of Cu-TCPP@Cu (Fig. 1d and Fig. S2a–c). This indicates that TCPP plays significant roles in regulating the morphology of Cu₂O.

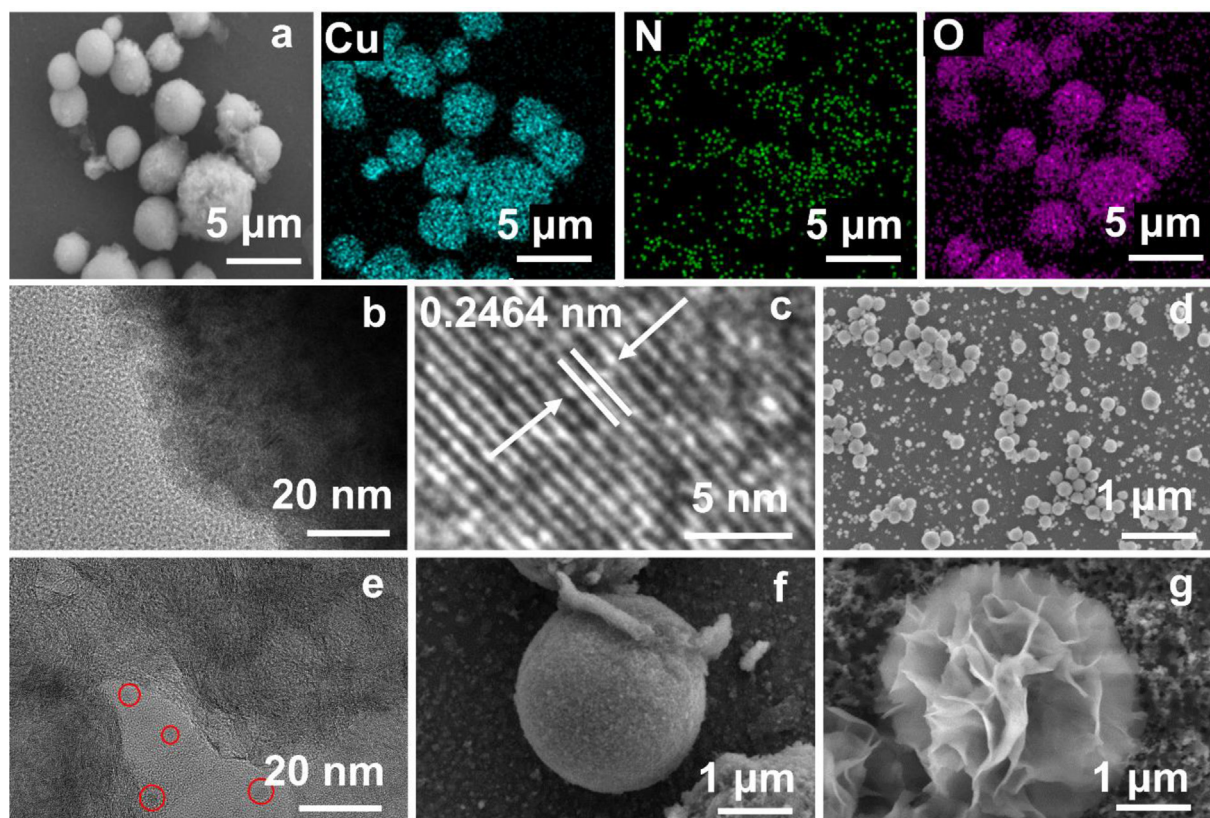


Fig. 1. The structural characterization: (a) SEM image of the Cu-TCPP@Cu₂O and the corresponding EDX mapping images of Cu, N, O, (b–c) TEM images of Cu-TCPP@Cu₂O and (d) SEM image of Cu₂O, (e) TEM image of Cu-TCPP@Cu/PC, (f) SEM image of Cu-TCPP@Cu and (g) SEM image of Cu-TCPP.

After an electrolysis at -1.0 V for 30 min, the Cu₂O nanoparticles were converted to metallic Cu, and the Cu nanoclusters with a diameter of about 3 nm on PC were observed for the Cu-TCPP@Cu/PC sample (Fig. 1e). Fig. 1f indicates that Cu-TCPP@Cu₂O retains its spherical structure even after the electrolysis. In contrast, the highly porous and aggregated Cu nanoparticles and nanowires at hundreds of nanometre scale were observed for the pure Cu₂O after the electrolysis (OD-Cu, Fig. S3a–3b). Apparently, Cu-TCPP can modulate not only the growth dynamics of Cu₂O, but also the recrystallization process of Cu during ECR process when Cu₂O is converted to Cu. Due to the strong interaction of Cu-TCPP and Cu, the structure of Cu-TCPP@Cu₂O was mainly maintained. SEM observation of Cu-TCPP fresh and Cu-TCPP spent (Figs. 1g and 3c–3d) also proves its structural stability. Cu-TCPP displays a nanoflower-like structure. After the electrolysis, the structure collapsed slightly but still maintained a flower-like structure in general. In Fig. S3e–3f, TCPP shows a severe aggregation both before and after the electrolysis.

As shown in Fig. 2 and Fig. S4, the peaks at 2θ values of 7.96, 11.03, 19.0 and 22.02° could be indexed to (110), (200), (004) and (400) reflection

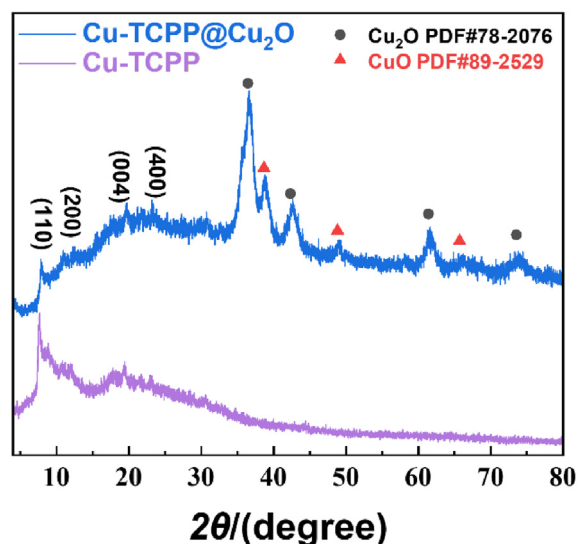


Fig. 2. XRD patterns of Cu-TCPP@Cu₂O and Cu-TCPP.

[47–50] of Cu-TCPP MOF, respectively, in Cu-TCPP@Cu₂O and Cu-TCPP both before and after the electrolysis. The peaks at 36.52, 42.32, 61.43 and 73.34° correspond to the crystal planes of (111), (200), (220) and (311) of crystalline Cu₂O, respectively [51], which are observed for both

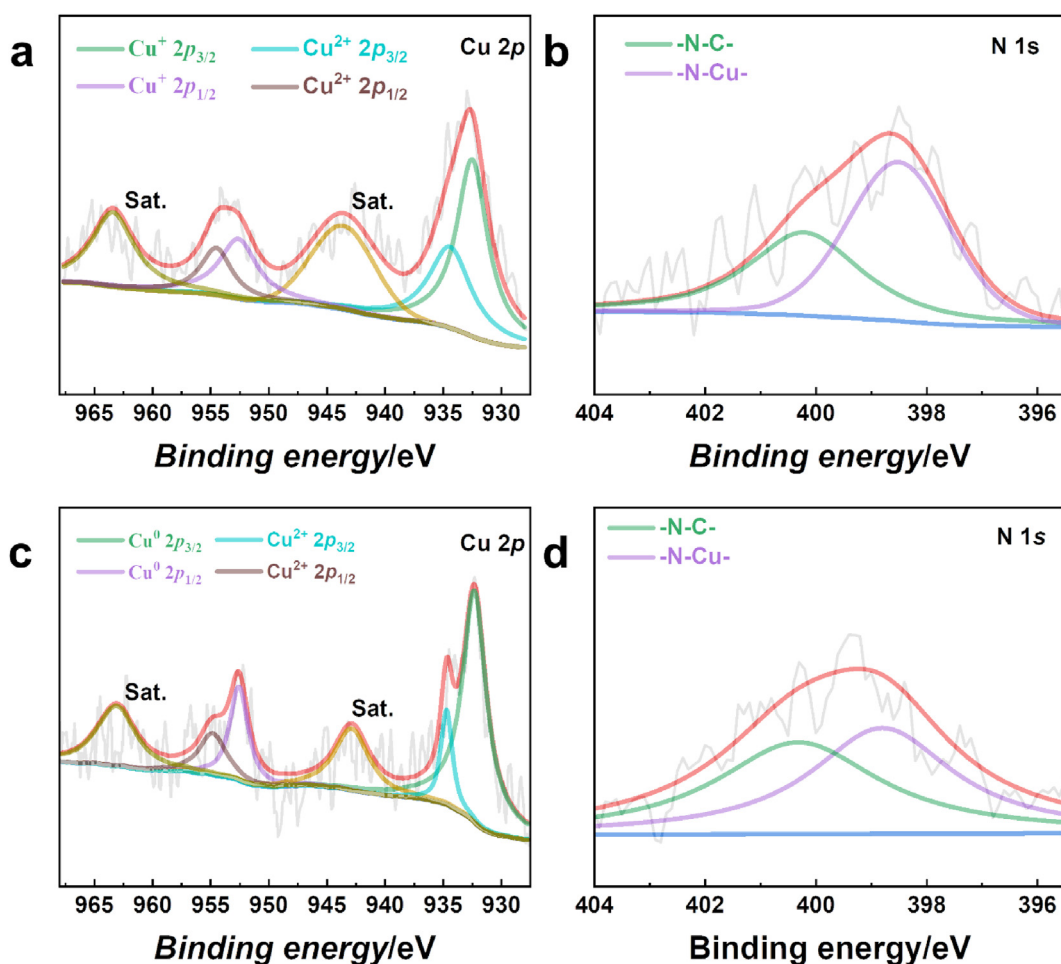


Fig. 3. XPS spectra of (a) Cu 2p, (b) N 1s for Cu-TCPP@Cu₂O/PC and (c) Cu 2p, (d) N 1s for Cu-TCPP@Cu/PC.

Cu-TCPP@Cu₂O and Cu₂O. In addition, the small peaks at 38.77, 48.84 and 65.73° might be indexed to CuO (PDF#89-2529).

Cu²⁺ may possibly not be completely converted into Cu⁺ during the preparation of catalyst, thus a small amount of CuO was remained in the catalyst. However, Cu₂O could still be dominant in the Cu-TCPP@Cu₂O. The XRD results indicate that the Cu-TCPP@Cu₂O represented the Cu-TCPP functionalized Cu₂O, while only the pure phase of Cu₂O was obtained without using TCPP in the synthetic procedure. After an electrolysis at -1.0 V, the characteristic peak of Cu₂O vanished from both Cu-TCPP@Cu₂O and Cu₂O, and only those diffraction peaks related to Cu were observed, signifying the complete conversion of Cu₂O to Cu at the ECR process. However, the diffraction peaks of Cu-TCPP were well maintained during the electrolysis, indicating its high stability against ECR process.

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Fig. 3a shows the Cu 2*p* spectrum for the as-prepared Cu-TCPP@Cu₂O. The binding energies at 932.5, 934.7 and 943.9 eV were assigned to Cu¹⁺ in Cu₂O, Cu²⁺ in CuO and Cu-TCPP, and the satellite of a Cu 2*p*_{3/2} peak, respectively [52,53]. Three peaks appeared at 952.4, 954.6, and 963.4 eV were attributed to Cu⁺ in Cu₂O, Cu²⁺ in CuO and Cu-TCPP, and the satellite of a Cu 2*p*_{1/2} peak, respectively [45,52,53]. In Fig. 3b, the N 1*s* spectra of Cu-TCPP@Cu₂O/PC observed at 400.3 eV and 398.8 eV could be accounted for pyridinic-N and Cu-N bond, respectively [50]. This further indicates the presence of Cu-TCPP in Cu-TCPP@Cu₂O composite. As shown in Fig. 3c, after the electrolysis, the satellite peak of Cu remained, which may come from Cu²⁺ species in Cu-TCPP [50]. This further confirms the integrity of Cu-TCPP against ECR electrolysis.

It should also be noted that the intensity of the Cu oxide satellite peak becomes much weaker than that of the fresh sample due to the conversion of Cu₂O to Cu. The binding energies at 932.5 and 934.7 eV were assigned to Cu⁰ and a few Cu²⁺ in the Cu-TCPP (a Cu 2*p*_{3/2} peak) [52–54]. Two peaks appeared at 952.4 and 954.6 eV were attributed to Cu⁰ and a few Cu²⁺ in the Cu-TCPP (a Cu 2*p*_{1/2} peak) [43]. In Fig. 3d, the N 1*s* spectra of Cu-TCPP@Cu exhibit a higher peak intensity of pyridinic-N and a lower peak intensity of Cu-N bond than those of Cu-TCPP@Cu₂O, possibly due to the partial breakage of Cu-N bond in Cu-TCPP, and conversion to metallic Cu and TCPP

[55–57]. However, according to the XRD and SEM results, the Cu-TCPP structure in Cu-TCPP@Cu₂O can generally remain stable after the electrolysis.

The LSV (Fig. 4a) curves were recorded in N₂ and CO₂ atmospheres in 1.0 mol·L⁻¹ KOH from 0 to -1.6 V. The current density of Cu-TCPP@Cu₂O/PC in CO₂ was higher than that in N₂, which indicates that the catalyst does have ECR activity. It was found that the products distribution of ECR over TCPP@Cu₂O/PC depends on the electrode potential (Fig. 4b). At -0.8 V and -0.9 V, C₁ product and H₂ became dominated in ECR. As the catalyst electrode was further negatively polarized to -1.0 V, the yields of ethanol and ethylene were dramatically increased, with ethylene being the dominant ECR product (Fig. 4b). C₂ product was the predominant ECR product for the Cu-TCPP@Cu₂O/PC catalyst at -1.0 V (Fig. 4b) and its FE reached 62.3%. In contrast, ECR was dominated by HER and CO on Cu₂O/PC (Fig. 4c), Cu-TCPP/PC (Fig. S5a) and TCPP/PC (Fig. S5b and Fig. S5c). These results indicate that the combination of Cu₂O and Cu-TCPP on PC is essential for efficient production of C₂ products in ECR.

In Fig. 4d, Cu-TCPP@Cu₂O/PC displays a supreme partial current density of C₂ products in the potential range of -0.8 V to -1.0 V, which is as high as 83.4 mA·cm⁻² and more than 7.6 times those of the unmodified Cu₂O, Cu-TCPP and TCPP. As shown in Fig. S5d and Fig. S6, the partial current density of C₁ (which is mainly CO) on Cu-TCPP@Cu₂O/PC was comparable to those of

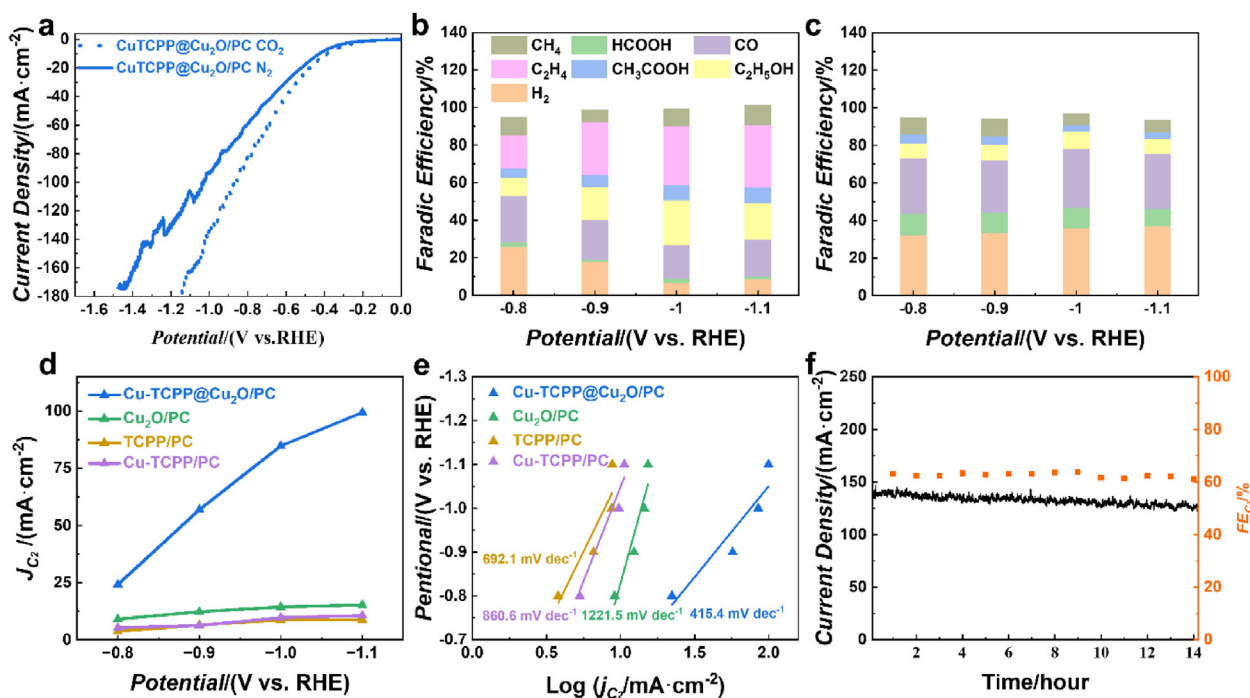


Fig. 4. ECR performance: (a) LSV of Cu-TCPP@Cu₂O/PC in CO₂ and N₂, Faradaic efficiencies for ECR products on (b) Cu-TCPP@Cu₂O/PC and (c) Cu₂O/PC across a potential range from -0.8 to -1.1 V vs. RHE, (d) Partial current density of C₂ and (e) Tafel plots for C₂ product of ECR on Cu-TCPP@Cu₂O/PC, Cu₂O/PC, Cu-TCPP/PC and TCPP/PC, respectively. (f) ECR stability assessment on Cu-TCPP@Cu₂O/PC at -1.0 V vs. RHE.

Cu₂O/PC and Cu-TCPP/PC but higher than TCPP/PC. It is further proved that the higher selectivity of C₂ product on Cu-TCPP@Cu₂O/PC can be obtained by C–C coupling of a large number of CO intermediates on Cu₂O/PC and Cu-TCPP/PC. Tafel slopes are calculated based on Tafel equation ($\eta = b \log j + a$, where η is the overpotential, j is the current density and b is the Tafel slope) [32] to elucidate the dynamics activity of catalyst for ECR (Fig. 4e). The Tafel slope for C₂ product on Cu-TCPP@Cu₂O/PC is 415.4 mV·dec⁻¹, which is much smaller than those of Cu₂O/PC (1221.5 mV·dec⁻¹), Cu-TCPP/PC (860.6 mV·dec⁻¹) and TCPP/PC (692.1 mV·dec⁻¹). The result states the favorable kinetics of Cu-TCPP@Cu₂O/PC for the formation of C₂ products.

It is highly possible that functionalization of OD-Cu with Cu-TCPP may enhance the hydrophobic properties of the catalyst composite, thus, suppressing the HER process. Additionally, both OD-Cu and Cu-TCPP here are good ECR catalysts for CO production, and the combination of Cu-TCPP and OD-Cu possibly enhances the local concentration of CO intermediates on OD-Cu surface, thus, promoting C–C coupling for C₂ production. According to earlier report [58,59], CO on Cu (2+) in Cu-TCPP and Cu (0) is also favorable to C–C coupling. All the three factors concurrently promote C₂ product in ECR process on Cu-TCPP@Cu₂O/PC catalyst. To examine the intrinsic activity of the catalysts, the electrochemical active surface area (ECSA) was evaluated by electrochemical double-layer capacitance (C_{dl}). Fig. S7–8 and Table S1 show that Cu-TCPP@Cu₂O/PC indeed exhibits larger C_{dl} value and ECSA than those of Cu₂O/PC, Cu-TCPP/PC and TCPP/PC, which provide more active sites in electrocatalyst to contact the electrolyte for ECR [29]. As shown in Fig. S9, the current density normalized to ECSA shows basically the same trend as in the geometric current density.

The Nyquist plots (Fig. S10) prove that Cu-TCPP@Cu₂O/PC has much smaller charge transfer resistance than Cu₂O/PC, Cu-TCPP/PC and TCPP/PC at the process of ECR, which indicates that Cu-TCPP@Cu₂O/PC can provide faster electron transfer from the catalyst surface to the reactant in intermediate generation, eventually resulting in largely enhanced activity and selectivity [60,61]. As shown in Fig. 4f, the faradaic efficiency of C₂ product is nearly 60% within 14 h at a potential of -1.0 V, indicating an outstanding ECR stability.

4. Conclusions

In this work, we have successfully prepared the uniformly distributed and spherical shaped Cu-

TCPP@Cu₂O organic/inorganic hybrid catalyst, which is composed of 2-dimensional Cu-TCPP ultrathin nanosheet and Cu₂O. It shows the excellent ECR performance toward production of C₂ products, with a faradaic efficiency of 62.3% at a flow cell in 1.0 mol·L⁻¹ KOH electrolyte. The Cu-TCPP@Cu₂O/PC catalyst had an inseparable interaction, which can effectively adsorb the intermediates, promoting the C–C coupling reaction and then improving the selectivity of C₂ products. This work highlights an effective strategy to design efficient Cu porphyrin-based MOF catalysts for electrochemical reduction of CO₂ into C₂ products.

Conflict of interest

There are no conflicts to declare.

Acknowledgements

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单分散 Cu-TCPP/Cu₂O 杂化微球:一种具有优异电还原 CO₂ 产 C₂ 性能的级联电催化剂

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摘要

高效电还原 CO₂ (ECR) 为有价值的多碳产物是解决 CO₂ 排放问题的有效解决方案。基于卟啉的金属有机框架 (MOFs) 具有多孔结构和有序的活性位点, 有望提高 ECR 生成多碳产物的选择性。本文制备了由铜-四(4-羧基)卟啉 (Cu-TCPP) 和 Cu₂O 组成的有机/无机杂化 Cu-TCPP@Cu₂O 电催化剂, 其中 TCPP 在调控形貌方面起着重要作用。ECR 过程中原位形成的 Cu 与 Cu-TCPP (Cu-TCPP@Cu) 结合可以抑制析氢, 富集 CO 中间体, 促进 C-C 偶联生成 C₂ 产物。多孔碳 (PC) 负载的 Cu-TCPP@Cu 在 PC 上被还原为 Cu 纳米簇, 同时对 C₂ 产物具有较高的 ECR 活性和选择性。催化剂在 -1.0 V 时 (相对于可逆氢电极), C₂ 产物法拉第效率为 62.3%, 部分电流密度为 83.4 mA·cm⁻², 是纯 Cu₂O 和 TCPP 的 7.6 倍和 13.1 倍。本论文研究了催化剂形貌和杂化结构如何提高 ECR 生 C₂ 产物的选择性, 为高性能 ECR 催化剂的设计提供了新思路。

关键字: 有机/无机杂化电催化剂; 四(4-羧基)卟啉; 氧化亚铜; 级联电催化剂